# A Chemical Conversion Hydroxyapatite Coating on AZ60 Magnesium Alloy and Its Electrochemical Corrosion Behaviour

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In order to improve the biodegradation properties of the magnesium alloy, a bioactive hydroxyapatite (HA) coating was deposited on AZ60 magnesium alloy by a two-step chemical method, i.e., dicalcium phosphate dihydrate (DCPD) coating was formed through a phosphating process, and then transformed to hydroxyapatite coating via alkali-heat treatment. SEM micrographs show that the HA coating is compact with the thickness of about  $6\mu$ m. Electrochemical tests were used to examine the corrosion performance in NaCl solution and simulated body fluid (SBF) and the results reveal that the HA coating significantly retards the corrosion rate of AZ60 alloy in both solutions.

Keywords: Magnesium alloy; Hydroxyapatite (HA) coating; Electrochemical corrosion.

# **1. INTRODUCTION**

Magnesium and its alloys have attracted considerable attention as potential implant materials in recent years [1-5]. Compared with ceramics, polymeric materials and other metal implants, magnesium alloys exhibit a combination of good mechanical properties, attractive biocompatibilities and biodegradation properties [1, 4, 6]. Thus, magnesium and its alloys could be good candidates as lightweight, degradable and load bearing orthopaedic implants [4, 7].

However, magnesium and its alloys corrode quickly in chloride containing solutions, e. g. the human body fluid or blood plasma [8]. So, if magnesium alloy is used as orthopaedic implant, its overrapid corrosion rate would make the implant not maintain mechanical integrity before the bone tissue has sufficiently healed. Several possibilities exist to tailor the corrosion rate of magnesium by using alloying elements and protective coatings. Compared with the alloying route, appropriate surface treatment can better match the tissue healing requirement of providing adequate mechanical support in the initial period of implantation and faster degradation when healing is near completion [9]. Although

a number of protective coatings, including oxidation coating [10], conversion coating [11] and stearic acid coating [12], have been achieved on magnesium and its alloys, these coatings do not satisfy both the biocompatibility and appropriate corrosion resistance for implant materials. In the aspect of biocompatible protective coatings, hydroxyapatite (HA,  $Ca_{10}(PO_4)_6(OH)_2$ ) is a preferential coating material, which has similar chemical and structural resemblance to natural bones and can accelerate bone concrescence [13]. There has been some research works about HA coatings on magnesium and its alloys with different methods, including biomimetic techniques [14, 15], chemical deposition [16, 17] and electrodeposition [18-20]. In most studies, pre-treatments in either alkaline solutions like NaOH [14] or acidic solutions of phosphoric acid [15] or HNO<sub>3</sub> [16] are required in order to modify the surface reactivity of the magnesium alloy substrate. Among the various surface treatments, chemical conversion deposition is conveniently and simply operated to produce a uniform and well adhered coating, especially for the complex-shaped components of the orthopaedic implant. A calcium phosphate conversion coating was carried out on the Mg-8.8Li alloy by Song et. al. [21], but the coating was not transformed to the biocompatible HA coating. Additionally, the Mg–Li alloy is not a good potential implant material, but commonly used in aerospace and military applications, and the formation mechanism of conversion film on Mg-Li alloy may be different from that on the conventional magnesium alloys.

So in the present study, we describe a simple two-step chemical method without external electrical circuit or any pre-treatment, to deposit a compact and well adhered HA coating on AZ60 alloy. The deposition mechanism of the coating was analysed; and the corrosion behaviour was investigated by the polarisation measurements in 3.5wt% NaCl solution and simulated body fluid (SBF).

#### 2. EXPERIMENTAL PROCEDURE

**Table 1.** The composition of AZ60 magnesium alloy (wt. %).



AZ60 die cast magnesium alloy was used as the substrate material; its composition is given in Table 1. The sample size was 12 mm×12 mm×5 mm. The sample surface was polished with up to 2000 grit SiC paper followed by sonication cleanout in acetone. The cleaned samples were immersed into a phosphating solution at  $37\pm2^{\circ}$ C for 30 min and were then dried in an attemperator at 60°C. The composition of the phosphating solution is given in Table 2, and its pH was adjusted by adding NaOH to 2.8-3.0. The dried samples were then alkali treated in 1M NaOH solution at 80°C for 2h to form the final coating.

The phase of the samples with and without coatings were characterized by X-ray diffraction (XRD, Rigaku Dymax, Japan) with a Cu K $\alpha$  radiation ( $\lambda$ =0.154178 nm) and a monochromator at 40

kV and 200 mA with the scanning rate and step being 4°/min and 0.02°, respectively. The morphologies and the composition of the coatings were identified by scanning electron microscopy (SEM, ZEISS EV018, Germany) equipped with energy dispersive X-ray spectrometer (EDS, X-Max, Oxford Instruments).

Table 2. The composition of t	he phosphating solution.
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Composition	Concentration
H <sub>3</sub> PO <sub>4</sub> (85% V/V)	8 mL/L
CaO	1.2 g/L
$Ca(NO_3)_2 \bullet 4H_2O$	11 g/L
Na <sub>2</sub> MoO <sub>4</sub> •2H <sub>2</sub> O	0.5 g/L

The corrosion resistances were evaluated by the electrochemical tests in 3.5wt% NaCl solution (20°C) and SBF (37°C), respectively. SBF is composed of 8.0 g/L NaCl, 0.4 g/L KCl, 0.14 g/L CaCl<sub>2</sub>, 0.35 g/L NaHCO<sub>3</sub>, 1.0 g/L C<sub>6</sub>H<sub>6</sub>O<sub>6</sub> (glucose), 0.2 g/L MgSO<sub>4</sub>·H<sub>2</sub>O, 0.1 g/L KH<sub>2</sub>PO<sub>4</sub>·H<sub>2</sub>O, 0.06 g/L Na<sub>2</sub>HPO<sub>4</sub>·H<sub>2</sub>O and pH=7.4 [6]. Electrochemical tests were performed on an Electrochemical Analyser (Versa STAT3, Princeton Applied Research) using a classical three electrodes cell with platinum as counter electrode, saturated calomel electrode SCE (+0.242 V vs. SHE) as reference electrode and the samples as working electrode (0.5 cm<sup>2</sup> exposed area). The scanning rate was 5 mV/s for all measurements. The data for potentiodynamic polarisation curves were analysed using the CorrView software developed by Scribner Associates, Inc. The surface morphologies of the three kinds of samples after the polarisation measurements were observed with SEM.

# **3. RESULTS AND DISCUSSION**

#### 3.1 Microstructure and phase composition



Figure 1. XRD patterns of (I) untreated, (II) phosphate treated, and (III) alkali treated surfaces of the magnesium alloy.



**Figure 2.** The surface and cross-sectional morphologies of (a-c) phosphate coating and (d-f) HA coating. (Insets) EDS results.

Fig. 1 shows the XRD patterns of the untreated, phosphate treated and alkali treated surfaces of the magnesium alloy. AZ60 magnesium alloy substrate mainly consists of  $\alpha$ -Mg solid solution, and without corrosion or pre-treatment the  $\beta$  phase was generally less detectable due to its small quantity [22]. After phosphating, the magnesium alloy substrate was covered mainly by dicalcium phosphate dihydrate (CaHPO<sub>4</sub>·2H<sub>2</sub>O, DCPD) and a small quantity of tricalcium phosphate (Ca<sub>3</sub>(PO<sub>4</sub>)<sub>2</sub>) and magnesium phosphate (Mg<sub>3</sub>(PO<sub>4</sub>)<sub>2</sub>), as shown by the XRD pattern II in Fig.1. After the alkali-heat

treatment, HA became the main phase with a certain quantity of magnesium hydroxide  $(Mg(OH)_2)$  in the coating.

The surface and cross-sectional morphologies as well as the EDS results of the phosphate coating and HA coating, are shown in Fig. 2 a, b c and d, e, f, respectively. A flake-like microstructure with flakes of 10-15 $\mu$ m in length appears on the surface of the phosphate coating (Fig. 2a). The line scanning of elements distribution across the coating and the substrate are depicted in Fig. 2c. The layer with significantly high Ca and P contents corresponds to the phosphate coating with an average thickness of about 6 $\mu$ m. The coating is not complete, with some caves or micro-pores between the flakes and beneath the coating surface (marked by arrows in Fig. 2c) being visible in the cross-sectional morphology.

As a precursor to HA, DCPD in the phosphate coating is unstable in environments with pH greater than 6~7 [8], hence the alkali-heat treatment was necessary to transform DCPD to HA, and meanwhile to make some flakes break off or dissolved (marked by an arrow in Fig. 2e), and then micro-pores disappeared (shown in the cross-sectional morphology of Fig. 2f). However, the average coating thickness is about 6µm and didn't change much after the alkali-heat treatment, as shown in Fig. 2f. This flake-like coating structure should be helpful for the bone tissue to infiltrate into the implants then to accelerate the healing of damaged bone [23]. The EDS results shown as insets in Fig. 2a and 2d indicate that the atomic percentage of Ca/P is 0.845 and 1.667 for the coating before and after the alkali-heat treatment, respectively, which are in agreement with the corresponding stoichiometric proportions of DCPD and HA, respectively.

## 3.2 Coating deposition process

In the phosphating process, both CaO and  $Ca(NO_3)_2 \cdot 4H_2O$  were added in the bath, which is different from the previous studies [21]. CaO reacted with H<sub>3</sub>PO<sub>4</sub>:

$$CaO + 2H_3 PO_4 \rightarrow Ca^{2+} + 2H_2 PO_4^- + H_2 O$$

$$\tag{1}$$

to form  $H_2PO_4^-$ , which is the major ion at pH<3[24]. The formation of phosphate coating on AZ60 alloy is related with the heterogeneity of magnesium alloy substrate. The sketch map of coating deposition is shown in Fig. 3. When the alloy was immersed into the phosphate bath, the substrate surface was divided into micro anodic sites and micro cathodic sites and the reactions on the surface should be thought to take place on different local polarisation sites correspondingly. Therefore, the following reaction can occur at micro anodic sites:

$$Mg \rightarrow Mg^{2+} + 2e^{-}$$
<sup>(2)</sup>

At the micro cathodic sites hydrogen evolution reaction occurred simultaneously:

$$H_2O + 2e^- \rightarrow 1/2H_2 + 2OH^-$$
(3)



Figure 3. The sketch map of coating deposition on AZ60 alloy.

The hydrogen generation reaction promoted the concentration of  $OH^-$  at the interface of metal and solution. Then  $OH^-$  reacted with  $H_2PO_4^-$  to form  $HPO_4^{-2-}$ :

$$H_2PO_4^- + OH^- \rightarrow HPO_4^{2-} + H_2O$$

$$\tag{4}$$

In the acidic phosphate bath, most  $HPO_4^{2-}$  preferentially bonded with  $Ca^{2+}$  to form insoluble CaHPO<sub>4</sub> ·2H<sub>2</sub>O:

$$Ca^{2+} + HPO_4^{2-} + 2H_2O \rightarrow CaHPO_4 \cdot 2H_2O$$
(5)

The reaction product CaHPO<sub>4</sub>  $\cdot$ 2H<sub>2</sub>O deposited on the magnesium alloy substrate to form the main ingredient of the phosphate coating. Some HPO<sub>4</sub><sup>-</sup> continued to react with OH<sup>-</sup> to form PO<sub>4</sub><sup>-</sup>, which would react with Ca<sup>2+</sup> from the bulk solution and Mg<sup>2+</sup> dissolved from the substrate (micro anodic sites) [21]:

$$HPO_4^- + OH^- \rightarrow PO_4^{2-} + H_2O \tag{6}$$

$$3Ca^{2+}+2PO_4^{2-} \rightarrow Ca_3(PO_4)_2 \tag{7}$$

$$3Mg^{2+}+2PO_4^{-} \rightarrow Mg_3(PO_4)_2 \tag{8}$$

The content of  $Mg_3(PO_4)_2$  in the phosphate coating was low due to the slow corrosive rate of AZ60 alloy in the phosphate solution.

Since the electrochemical potentials of  $\alpha$  phase ( $\alpha$ -Mg) and  $\beta$  phase (Mg<sub>17</sub>Al<sub>12</sub>) are different, and the hydrogen evolution on  $\beta$  phase is easier than that on  $\alpha$  phase [25],  $\beta$  phase is regarded as micro cathodic sites primitively. Thus, the coating was mainly deposited on  $\beta$  phase and only a spot of them was deposited on  $\alpha$  phase, as shown in Fig. 3b. When  $\beta$  phase was covered by phosphate coating, the hydrogen evolution on  $\beta$  phase became difficult. It is known that  $\alpha$  phase consists of magnesium and aluminium. Due to the solute redistribution in the dendritic solidification process and the segregation, aluminium content in primary  $\alpha$ -Mg and eutectic  $\alpha$ -Mg is different [26, 27]. So, it was electrochemically inhomogeneous at the interior of  $\alpha$  phase and micro-anodes and micro-cathodes could be identified. The sites containing more magnesium (e. g., primary  $\alpha$ -Mg) were the microanodes and the sites containing more aluminium (e. g., eutectic  $\alpha$ -Mg) were the microcathodes. In the case that  $\beta$  phase was probably covered by phosphate coating, the depositing process would continue at the micro cathodic sites of  $\alpha$  phase, as shown in Fig. 3c.

Additionally, the hydrogen gas was also generated from micro anode sites accompanying with the dissolution of magnesium at corroding area as proposed by Song [27, 28].

$$Mg \rightarrow Mg^+ + e^- \tag{9}$$

$$Mg^{+}+H_{2}O \rightarrow Mg^{2+}+OH^{-}+1/2H_{2}$$
(10)

So the coating continued to deposit at the corroding area following the reactions (4)–(8). Finally, the alloy was totally covered with phosphate coating as shown in Fig. 3d.

But the phosphate coating was still thin and the phosphating solution was easy to penetrate the incompact coating at some weak sites to slowly corrode the substrate, hence the coating grew continuously until the dynamic balance between substrate dissolution and coating formation was established, as shown in Fig. 3e.

In the present study, both  $Ca(NO_3)_2 \cdot 4H_2O$  and  $Na_2MoO_4 \cdot 2H_2O$  were used as accelerators. In the bath,  $NO_3^-$  and  $MoO_4^{2^-}$  ions reacted with H<sup>+</sup> in the solution-substrate boundary [21, 24,29]:

$$NO_3^{-}+2H^{+}+2e^{-} \rightarrow NO_2^{-}+H_2O$$
(11)

$$MoO_4^{2^-}+8H^++3e^- \rightarrow Mo^{3^+}+4H_2O$$
 (12)

These reactions also consumed  $H^+$  to promote the local pH value, which was beneficial to the formation of phosphate coating. Molybdate could also bond with  $Mg^{2+}$ , promoting formation of the coating [29, 30]:

$$Mg^{2+} + MoO_4^{2-} \rightarrow MgMoO_4$$
(13)

After the phosphate coating was obtained, the samples were immersed in the NaOH solution to transform DCPD to HA following the reaction:

$$10CaHPO_4 \cdot 2H_2O + 12NaOH \rightarrow Ca_{10}(PO_4)_6(OH)_2 + 4Na_3PO_4 + 12H_2O$$
(14)

The minor ingredient of the phosphate coating reacted with the alkali solution as well:

$$10Ca_{3}(PO_{4})_{2}+6NaOH \rightarrow 3Ca_{10}(PO_{4})_{6}(OH)_{2}+2Na_{3}PO_{4}$$

$$(15)$$

$$Mg_{3}(PO_{4})_{2}+6NaOH \rightarrow 3Mg(OH)_{2}+2Na_{3}PO_{4}$$
(16)

In the process of alkali-heat treatment, there was no bubble produced, which was different from the phosphating process. The alkali solution penetrated the incompact phosphate coating to dissolve some flakes and then most caves and micro-pores would be filled with the reaction products. Therefore, the coating became more compact and better adhered onto the substrate, as shown in Fig. 3f.

## 3.3 Measured polarisation behaviour



Figure 4. Potentiodynamic polarisation curves in (a) 3.5wt% NaCl solution and (b) SBF, respectively.

Fig. 4(a) and (b) show the potentiodynamic polarisation curves of the untreated AZ60 alloy, phosphate coating and HA coating in 3.5wt% NaCl solution (20°C) and SBF (37°C), respectively. The corrosion current density ( $I_{corr}$ ), and the anodic and cathodic Tafel slope ( $\beta_a$  and  $\beta_c$ , respectively) are simultaneously derived by curve fitting method using Corrview software based on the Butler and Volmer equation [31]:

$$I = I_{\rm corr} \left\{ \exp\left[\frac{2.303}{\beta_{\rm a}} \left(E - E_{\rm corr}\right)\right] - \exp\left[\frac{2.303}{\beta_{\rm c}} \left(E - E_{\rm corr}\right)\right] \right\}$$
(17)

where  $E_{\text{corr}}$  is the corrosion potential. The polarisation resistance ( $R_{\text{p}}$ ) can be evaluated from the Stern and Geary relationship [32]:

$$R_{\rm p} = \frac{\beta_{\rm a}\beta_{\rm c}}{2.303I_{\rm corr}\left(\beta_{\rm a} + \beta_{\rm c}\right)} \tag{18}$$



**Figure 5.** The surface morphologies of (a, d) untreated AZ60 alloy, (b, e) phosphate coating and (c, f) HA coating after the potentiodynamic polarisation measurements in (a-c) 3.5wt% NaCl solution and (d-f) SBF, respectively.

The pitting potential  $E_{pt}$  is equal to the inflexion potential on polarisation curves. When the polarisation potential exceeds  $E_{pt}$ , the corresponding current density has an abrupt drop in the cathodic branch or an abrupt increase in the anodic branch, which indicates the breakdown of the surface coating and the initiation of pitting corrosion. The values of all the electrochemical parameters obtained from the polarisation curves are listed in Table 3. The surface SEM morphologies of the samples after the potentiodynamic polarisation measurements are shown in Fig. 5. For the untreated alloy immersed in either NaCl or SBF solution, numerous bubbles were formed at the sample surface during the recording of the polarisation curve. The cathodic Tafel slope  $\beta_c$  is -206 mV/dec in NaCl solution and -221 mV/dec in SBF, respectively. These values are in the range of -120 to -300 mV/dec, which were found for the cathodic process of water or proton reduction with hydrogen release (Eq. (3)) [28, 33, 34]. So, the activation-controlled cathodic process occurred in the cathodic branch is mainly corresponding to the evolution of the hydrogen. An abrupt drop in the cathodic current density is observed in the cathodic branch of the curve close to the corrosion potential, which actually corresponds to the initiation of pitting corrosion. When the applied potential increased into the anodic branch, an activation-controlled anodic process was observed. The anodic branch is characteristic of a

corrosion process and is assigned to the dissolution of magnesium (Eq. (2)). The anodic Tafel slope  $\beta_a$  is 65 mV/dec in NaCl solution and 48 mV/dec in SBF, respectively. These values are in agreement with those obtained in the previous studies where the value varies from 30 mv/dec to 320 mv/dec [33, 35, 36]. The untreated alloy was attacked and dissolved, and the attack morphology changed from pitting corrosion to overall corrosion with the increase of applied potential without passivation. The surface was totally covered with big cracks, concave pits and the corrosion products (Fig.5 (a) and (d)), implying that severe corrosion occurred on the surface and corrosion products in pits were detached away into solution. This anodic behaviour at high potentials is partially controlled by mass transport, in agreement with previous studies [33-36].

**Table 3.** (i) Corrosion potential ( $E_{corr}$ ), (ii) corrosion current density ( $I_{corr}$ ), (iii) anodic and cathodic Tafel slope ( $\beta_a$  and  $\beta_c$ ), (iv) polarisation resistance ( $R_p$ ), and (v) pitting potential ( $E_{pt}$ ), derived from the polarisation curves (Fig. 4).

	<i>E</i> <sub>corr</sub> (V/SCE)	$I_{\rm corr}$ ( $\mu {\rm A/cm}^2$ )	$\beta_{a}$ (mV/dec)	$\beta_{\rm c}$ (mV/dec)	$R_{ m p}$ ( $\Omega \cdot  m cm^2$ )	E <sub>pt</sub> (V/SCE)
3.5wt% NaCl (20°C)						
Untreated AZ60	-1.51	105	65	-206	204	-1.53
Phosphate coating	-1.36	2.01	524	-121	21236	-0.98
HA coating	-1.28	0.37	201	-110	83432	-0.94
SBF (pH=7.4,						
37°C)						
Untreated AZ60	-1.43	33	48	-221	519	-1.44
Phosphate coating	-1.40	13	776	-149	4175	-1.2
HA coating	-1.31	0.82	234	-104	38126	-1.14

For the phosphate coating, the corrosion potential  $E_{corr}$  shows a significant shift to the positive direction, the polarisation current density  $I_{corr}$  decreases largely, and the polarisation resistance  $R_p$  increases significantly, compared with the untreated samples. Bubbles formation was reduced at the sample surface during the recording of the polarisation curve. An obvious passivation occurred in the anodic branch. The passivation range reached to 300 mV in NaCl solution and 120mV in SBF, respectively. Below the pitting potential the anodic plot has a very high slope, and then the anodic Tafel slope decreases abruptly, probably revealing the pitting of the substrate in parallel with the Mg oxidation. The corroded surface morphologies (Fig. 5(b) and (e)) show the characteristics of pitting corrosion, but only when the applied anodic potential exceeds the pitting potential  $E_{pt}$  to break the passive coating, did pitting corrosion occur.

For the HA coating, more evident protective effects are observed: the corrosion potentials  $E_{corr}$  show significant shifts to the positive direction, the corrosion current densities  $I_{corr}$  are estimated to be

as much as two decades lower, the polarisation resistance  $R_p$  is about two decades higher, and the pitting potentials  $E_{pt}$  show significant shifts of about 600mV in the NaCl solution and 300 mV in SBF, respectively, compared with the values of the untreated alloy. The cathodic Tafel slope  $\beta_c$  increases to about -100 mV/dec, resulting in few bubbles formation at the sample surface during the polarisation measurements. Although the anodic Tafel slope  $\beta_a$  is lower than that of the phosphate coating, the increased values of pitting potential  $E_{pt}$  indicate the HA coating can provide protection for the magnesium alloy in a large potential range, which was confirmed by corrosion morphologies in Fig. 5c and f. Only a few pits were observed with increasing anodic potential, especially in the NaCl solution (Fig. 5c). So the alkali-heat treatment for the phosphate coating leads to the formation of a well protective HA coating.

Table 4. The electrochemical	parameters value	es of several HA	A coatings in the	present study	and Ref.
[16-19].					

Coating /Substrate	Corrosive mediums	<i>E</i> <sub>corr</sub> (V/SCE)	$\frac{I_{\rm corr}}{(\mu {\rm A/cm}^2)}$
HA on AZ60 [present]	3.5wt% NaCl	-1.28	0.37
HA on AZ60 [present]	SBF	-1.31	0.82
HA on Mg [16]	3.5wt% NaCl	-1.65	0.28
HA on Mg [17]	MEM	-1.54	2.7
HA on Mg-Zn-Ca [18]	SBF	-1.41	25
HA on AZ91D [19]	SBF	-1.5	30

Different approaches have been explored to generate the HA coating on the magnesium alloys as well as pure magnesium in the previous studies [14-19]. The electrochemical parameters values of several HA coatings are summarized and compared with that of present study in Table 4. In spite of the different coating substrates, the corrosion potential  $E_{corr}$  is in the -1.4 to -1.65 V/SCE range and the corrosion current density  $I_{corr}$  varies from 0.28 to  $30\mu$ A/cm<sup>2</sup> in the previous studies [16-19]. By comparison, the corrosion potential ( $E_{corr}$ ) of the present study is the most positive one in both solutions and the corrosion current densities ( $I_{corr}$ ) are in the better range of less than  $1\mu$ A/cm<sup>2</sup>. Thus it can be confirmed that the present compact coating exhibits the better electrochemical corrosion resistance to protect the substrate in both NaCl and SBF solutions.

## 3.4 Theoretical polarisation behaviour

Fig. 6 schematically illustrates the magnesium dissolution and hydrogen evolution processes by comparing the theoretically decomposed polarisation curves (Fig. 6(a) and (b)) and the theoretically composed polarisation curves (Fig. 6(c)) of untreated AZ60 alloy, phosphate coating and HA coating

sample. The features of the measured polarisation curves possibly can be interpreted by theoretical polarisation behavior. The theoretically composed polarisation current always results from the combination of the theoretically decomposed anodic and cathodic polarisation currents:

$$I = \left| I_{\rm a} - I_{\rm c} \right| \tag{19}$$

For the untreated alloy (Fig. 6a), the surface is not corroded at first, so the hydrogen evolution and magnesium dissolution processes proceed in normal electrode behaviour. The magnesium dissolution increases (D–E) and the hydrogen evolution decreases (A–B) with the increasing polarisation potential [37].



**Figure 6.** Schematic illustration of the theoretical polarisation behaviours. (a) (b) theoretically decomposed polarisation behaviours; (c) theoretically composed polarisation behaviours.

As a result, the composed polarisation current decreases as polarisation potential becomes more positive before  $E_{pt}^{alloy}$  according to Eq. (19). A film containing mainly Mg(OH)<sub>2</sub> and MgO could formed soon after the immersion in the corrosive medium due to the low rate of the magnesium dissolution processes [38]. This thin film breaks down at a potential more negative than the corrosion potential. This normal phenomenon for Mg alloys indicates that the hydroxide/oxide layer is not a real passive film. When the polarisation potential is higher than  $E_{pt}^{alloy}$ , pitting corrosion occurs, which can be characterised by the dramatic increase of the rates of magnesium dissolution (E–F) and hydrogen evolution (B–C). The increasing rate of hydrogen evolution with potential is an important feature of the negative difference effect, which is always accompanied by dramatic dissolution of magnesium [39]. Thus, on the corroding surface both  $I_a$  and  $I_c$  increase with the increase of applied potential, resulting in suddenly decreasing I at a faster rate (Fig. 6c). This explains the abrupt drop in the

cathodic polarisation curves of the untreated alloy in Fig. 4. The intersecting point G between the curves A–B and D–E represents the corrosion potential  $E_{corr}^{alloy}$ . It should be noted that A–B and D–E actually represent hydrogen evolution and magnesium dissolution from the uncorroded surface, while B–C and E–F mainly represent hydrogen evolution and magnesium dissolution from the corroding area of the sample [37].

For the phosphate coating (Fig. 6a), only a relatively small area of the substrate can be attacked by corrosive medium due to the barrier function of the coating. So, the rates of the magnesium dissolution (K–L) and the hydrogen evolution (H–I) in the uncorroded area should be lower than that of the untreated AZ60 alloy. The stable corrosion resistant of the coating leads to a more positive pitting corrosion potential  $E_{pt}^{phosphate}$  (point L or I), which is even more positive than its corrosion potential  $E_{corr}^{phosphate}$  (the intersecting point N). While the polarisation potential is higher than  $E_{pt}^{phosphate}$ (point L or I), the rates of the magnesium dissolution (L–M) and the hydrogen evolution (I–J) in the corroding area increase dramatically. However, both the rates are lower than that of the untreated alloy due to the smaller corroding area. Both  $I_a$  and  $I_c$  increase with potential on the corroding surface, resulting in suddenly increasing I at a faster rate (Fig. 6c). This explains the abrupt increase in the anodic polarisation curves of the phosphate coating in Fig. 4.

For the HA coating (Fig. 6b), the relative positions of O–P, P–Q, R–S and S–T are slightly different from those of the phosphate coating. Micro-pores and gaps between flakes of the phosphate coating were buried after the alkali-heat treatment (Fig.2(c) and (f)). Compared with the phosphate coating, the more compact and better adhered HA coating makes less area of the substrate exposed to corrosive medium, which leads to the lower rates of the hydrogen evolution (H–I–J) and the magnesium dissolution (K–L–M) in the uncorroded area and the corroding area. As a result, the corrosion potential  $E_{corr}^{HA}$  (point W) and the pitting corrosion potential  $E_{pt}^{HA}$  (point S or P) are positive to these of the the phosphate coating, respectively.

In summary, the HA coated sample shows the optimal corrosion resistance, which can be attributed to the compact and well adhered coating formed on the substrate. Due to the effective protection for the AZ60 alloy substrate, the HA coating has potential applications for protecting degradable implants from rapid degradation. The biocompatibility of the coating is not evaluated

although there are no toxic elements in the coating. So, further investigations such as in vitro cell culture and in vivo animal tests are needed in future.

# 4. CONCLUSIONS

1) The compact and well adhered HA coating of about 6µm thick was deposited on the surface of AZ60 alloy by a two-step chemical method without external electrical circuit or any pre-treatment. The phosphate coating mainly consisted of DCPD was transformed into HA coating after the alkaliheat treatment.

2) The coating can serve as a physical barrier between the substrate and the aggressive environment, resulting in the low rates of magnesium dissolution and hydrogen evolution at different polarisation potential.

3) The present coating exhibits a better electrochemical corrosion resistance in comparison with the previous HA coatings.

4) The corrosion morphology observation after the potentiodynamic polarisation measurements also indicates that the HA coating can efficiently protect magnesium substrate from corrosion attack.

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