

# Highly Effective PdCu Electrocatalysts Supported on Polyelectrolyte Functionalized Titanium Dioxide for Direct Formic Acid Fuel Cells

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Received: 25 October 2016 / Accepted: 12 December 2016 / Published: 30 December 2016

A highly efficient and CO tolerant PdCu electrocatalysts supported on amino-rich, cationic poly(diallyl dimethyl ammonium chloride)(PDDA) functionalized TiO<sub>2</sub> (PdCu/TiO<sub>2</sub>(P)-C) has been developed. The catalysts were characterized by transmission electron microscopy (TEM), X-ray diffraction (XRD), cyclic voltammograms and chronoamperometry. The PdCu particles with average size ~3.5 nm are well dispersed on TiO<sub>2</sub>(P). PdCu/TiO<sub>2</sub>(P)-C catalysts exhibit a superior electrocatalytic activity and stability for the formic acid oxidation reaction compared with the Pd/TiO<sub>2</sub>(P)-C. Electrochemical measurements indicate that PdCu/TiO<sub>2</sub>(P)-C(1:2) catalyst has the best performance for formic acid electro-catalytic oxidation in terms of durability and Pd-mass activity among three catalysts (Pd<sub>1</sub>Cu<sub>1</sub>, Pd<sub>1</sub>Cu<sub>2</sub>, Pd<sub>1</sub>Cu<sub>3</sub>). The possible reason is that the addition of Cu is beneficial to lower appropriately the d-band center of Pd and increase the electrochemical active surface area of the PdCu/TiO<sub>2</sub>(P)-C nanocatalysts, but when the content of Cu rises to a certain extent, the morphology of the catalyst nanoparticles will transform into linear structure leading to increased particle size.

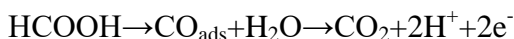
**Keywords:** Formic acid fuel cells; PdCu; electrocatalysts; titanium dioxide

## 1. INTRODUCTION

Direct formic acid fuel cells (DFAFCs) have many advantages, such as fast anode kinetics (similar with hydrogen PEMFCs), easy fuel storage and a higher theoretical voltage. Furthermore, formic acid exhibits low permeability through Nafion® membrane, which allows high concentrations of formic acid (up to 15 M) to be used in fuel cells. For these reasons, DFAFCs have received great attention[1-3].

Pd/C and Pt/C are the two main catalysts for the formic acid electrochemical oxidation among the anode catalysts in DFAFCs[4-5]. A dual pathway reaction mechanism has been proposed and

widely recognized for the electrochemical oxidation of formic acid[6-7]. One path was known as the direct path, which involves the direct oxidation of formic acid to carbon dioxide.



while another path relates to an inhibiting intermediate like adsorbed carbon monoxide ( $\text{CO}_{\text{ads}}$ ), which produced from the dehydration of formic acid (indirect path). The inhibiting intermediate results in severe poisoning of the catalyst. Over Pt/C catalysts, formic acid oxidizes primarily through the indirect pathway. On the other hand, Pd/C catalysts oxidize formic acid mainly through the direct pathway, where the forming of CO intermediate is suppressed. Therefore, researchers generally believe that Pd/C catalyst is the more desirable catalyst for the electrochemical oxidation of formic acid[8]. However, even though the formic acid is mainly oxidized via the direct pathway on the Pd/C catalysts, a small amount of formic acid still can be oxidized via the indirect pathway. Consequently,  $\text{CO}_{\text{ads}}$  slowly accumulates over the Pd catalysts, which leads to the poor long-term stability of the catalysts[9]. In addition, Pd is a noble metal and very expensive. So, it is necessary to improve its overall electrochemical performance and develop less expensive Pd-based catalysts.

In order to further improve the electrocatalytic performance of the Pd catalysts, the Pd-based bimetallic and trimetallic catalysts have been investigated, such as PdNi[10], PdCo[11], PdFe[12], PdCuIr[13], PdCoIr[14] and PdNiCu[15]. Bimetallic and trimetallic catalysts usually show better performance than monometallic catalysts because the addition of the second element usually decreases the Pd d-band center, which results in the weakening of the adsorption of reaction intermediates[16-17].

It is well known that support exerts an important impact on the performance of fuel cell catalyst[18]. Carbon black is generally used to support noble metal in catalyst. Nevertheless, carbon materials are corroded easily in the environment of fuel cell, which will lead to the aggregation of Pd nanoparticles and result in the deterioration of catalyst performance[19]. Many researchers use non-carbon materials as catalyst support to solve this problem. For example, TiN[20],  $\text{WO}_x$ [21], WC[22] and  $\text{SiO}_2$ [23]. In our previous research, we also found that the use of  $\text{TiO}_2$  as a catalyst support improves the activity and stability of the catalyst[24]. Recently, we developed a strategy to prepare highly dispersed Pd nanoparticles supported on  $\text{TiO}_2$  modified by poly(diallyl dimethyl ammonium chloride)(PDDA), where PDDA employed as effective functional agents for the self-assembly of  $\text{PdCl}_4^{2-}$  and in situ deposition on the surface of  $\text{TiO}_2$ [25].

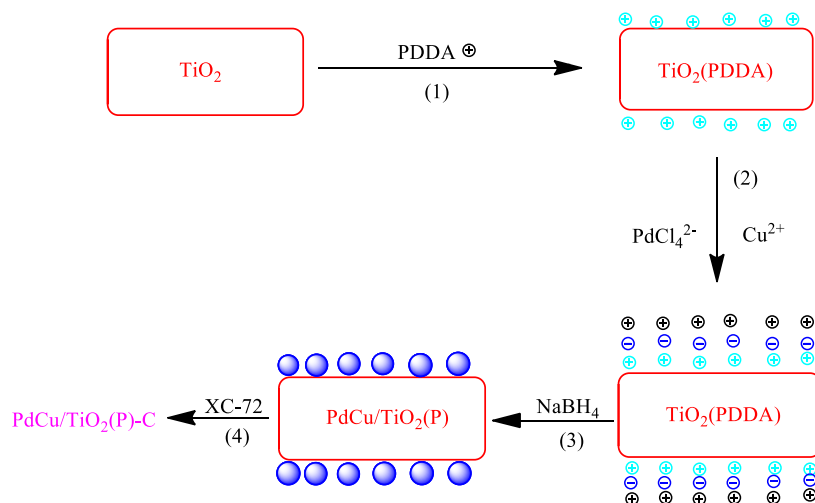
Based on our previous researches, PdCu/ $\text{TiO}_2$ (P)-C catalysts with different mass ratios of Pd and Cu are prepared in this paper by the self-assembly between the positively charged PDDA, negatively charged Pd and the positively charged Cu precursor, and then in situ deposition on the surface of  $\text{TiO}_2$  modified by PDDA, aiming to have a less expensive electro-catalyst in the DFAFC. The particle size and dispersion of the supported PdCu catalysts were obtained by transmission electron microscopy (TEM). High resolution transmission electron microscopy (HRTEM) and X-ray diffraction (XRD) measurements confirmed the alloy formation. Cyclic voltammetry (CV) and chronoamperometry (CA) were used to measure the activity and stability of these Pd-based catalysts toward the electro-chemical oxidation of formic acid.

## 2. EXPERIMENTAL SECTION

Materials used in this research, such as sulfuric acid ( $\text{H}_2\text{SO}_4$ ), and hydrochloric acid ( $\text{HCl}$ ), formic acid ( $\text{HCOOH}$ ), palladium chloride ( $\text{PdCl}_2$ ), Copper sulfate pentahydrate ( $\text{CuSO}_4 \cdot 5\text{H}_2\text{O}$ ), sodium borohydride ( $\text{NaBH}_4$ ), trisodium citrate ( $\text{Na}_3\text{C}_6\text{H}_5\text{O}_7 \cdot 2\text{H}_2\text{O}$ ), were purchased from Sinopharm Chemical Reagent Co., Ltd. All reagents, unless stated otherwise, were of analytical reagent grade and can be used directly. Anatase- $\text{TiO}_2$  (particle size = 15~20 nm) and poly (diallyl dimethyl ammonium chloride) (PDDA, average MW: 100,000~200,000) were obtained from Aladdin Industrial Corporation. VXC-72 carbon black ( $S_{\text{BET}} = 240 \text{ m}^2 \cdot \text{g}^{-1}$ ) was purchased from Cabot and then refluxed in 5M  $\text{HNO}_3$ . Water used was always deionized water.

### 2.1. Catalysts preparation

For the catalyst preparation,  $\text{TiO}_2$  firstly treated by PDDA. The process of non-covalent functionalization of  $\text{TiO}_2$  with PDDA can be described as follows. Firstly, 200 mL of 0.5 wt.% PDDA aqueous solution was prepared, which acted as the functionalization polyelectrolyte. After that, 1 g of pristine  $\text{TiO}_2$  was dispersed in it and keep the solution in ultrasonic treatment for 1 h. Then, 4 g NaCl was added into the above solution and being stirred for overnight. The Addition of NaCl is for increasing the ionic strength of solution and the attractive force between PDDA and the  $\text{TiO}_2$  surface, thus resulting in higher functionalization degree on  $\text{TiO}_2$ . Finally, the solution was filtrated and washed using deionized water for many times to move away the redundant PDDA. Than the material retained on the filter was dried at  $80^\circ\text{C}$  for 10 h in vacuum to obtain  $\text{TiO}_2(\text{P})$ .



**Figure 1.** The preparation process of PdCu/TiO<sub>2</sub>(P)-C

Weigh a certain amount of  $\text{TiO}_2(\text{P})$  and  $\text{Na}_3\text{C}_6\text{H}_5\text{O}_7 \cdot 2\text{H}_2\text{O}$ , and dispersed in water. Then, a stoichiometric amount of  $\text{H}_2\text{PdCl}_4$  solution ( $\text{PdCl}_2$  dissolved in 0.1 M  $\text{HCl}$ ) and  $\text{CuSO}_4$  aqueous solution was added in the mixture, and kept stirring for 12 hours before dropwise adding excessive

amounts of 0.01 M freshly prepared  $\text{NaBH}_4$  under ice-water conditions. After that, the carbon slurry was added into the above mixture, which was still stirred continually. After 10 min of stirring, the mixture was filtered and then washed with deionized water for many times, which is in order to completely ensure all excess reducing agents were completely removed. Finally, the remained solids were dried in vacuum for 12 h at  $80^\circ\text{C}$ . PdCu/TiO<sub>2</sub>(P)-C catalysts with different mass ratios of Pd and Cu denoted as PdCu/TiO<sub>2</sub>(P)-C(1:1)、PdCu/TiO<sub>2</sub>(P)-C(1:2)、PdCu/TiO<sub>2</sub>(P)-C(1:3) and Pd/TiO<sub>2</sub>(P)-C were prepared by the above method and the metal content of all four catalysts theoretically was 20% . The preparation process is demonstrated in figure.1.

## 2.2 Characterization of catalysts

TEM micrographs of all catalysts were taken on JEM-3010 transmission electron microscope, which operated under the condition of 0.17 nm spatial resolution and 300 kV voltage. Firstly, the catalysts were ground into fine particles, and then well dispersed in alcohol for ultrasonic treatment. After that, a drop of the dispersion was transferred onto a standard carbon-film-coated copper grid to take electron micrographs.

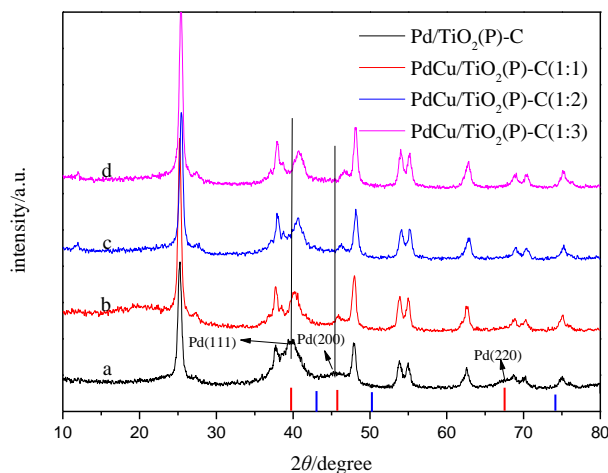
XRD patterns of all researched catalysts were obtained by the SHIMADZU (XRD-6100) diffractometer with Cu K $\alpha$  irradiation at 40 kV and 30 mA. The angular resolution ( $2\theta$ ) of the diffractometer was  $0.05^\circ$  and the scan rate was  $4^\circ\cdot\text{min}^{-1}$ .

## 2.3 Electrode preparation and measurement

Glassy carbon electrode with 5 mm of diameter was used as the underlying substrate of the working electrode. Before using in each experiment, this glassy carbon electrode was polished successively with 0.3  $\mu\text{m}$  and 0.05  $\mu\text{m}$  alumina slurry to have the high mirror finish. The catalysts were loaded onto the underlying substrate as follows. The dilute suspension of catalysts was fully dispersed under the condition of ultrasonic vibration, after that 10  $\mu\text{L}$  of the dispersed catalyst suspension was dropped onto the surface of polished glassy carbon electrode. After electrode dried, 10  $\mu\text{L}$  of Nafion, which was 5 wt.% dilute solution mixed Nafion with ultrapure water and lower aliphatic alcohols, was dropped onto the electrode surface.

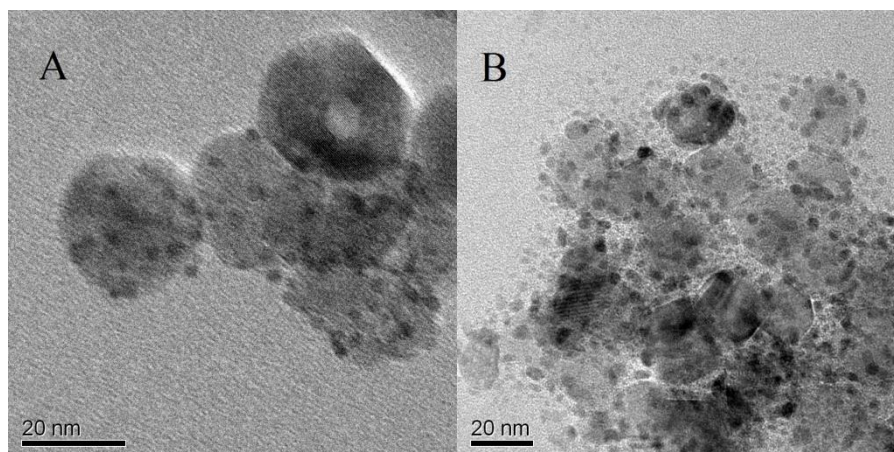
All electrochemical measurements were conducted using the Ingsens 3040 electrochemical workstation, which linked with an SAMSUNG PC, in a conventional three-electrode system at  $25^\circ\text{C}$ . In this experiment, the Pt net ( $1\text{ cm}^2$ ) was used as the counter electrode. Saturated calomel electrode (SCE) selected as reference electrode in this work. Prior to each measurement, ultrapure argon was kept bubbling into the 0.5 M  $\text{H}_2\text{SO}_4$  with or without 0.5 M  $\text{HCOOH}$  for 20 min as the electrolyte solution. The cyclic voltammograms (CV) curves were measured at voltages ranged from - 0.2 V to 1.0 V. The working electrode was treated with constantly cycling at  $50\text{ mV}\cdot\text{s}^{-1}$  with voltages ranged from -0.2 V to 1.0 V prior to each measurements, which is for removing any possible contaminants on Nafion membrane and Cu on the surface. Keep all electrodes processed for the same time until gaining a stable response of each working electrode .

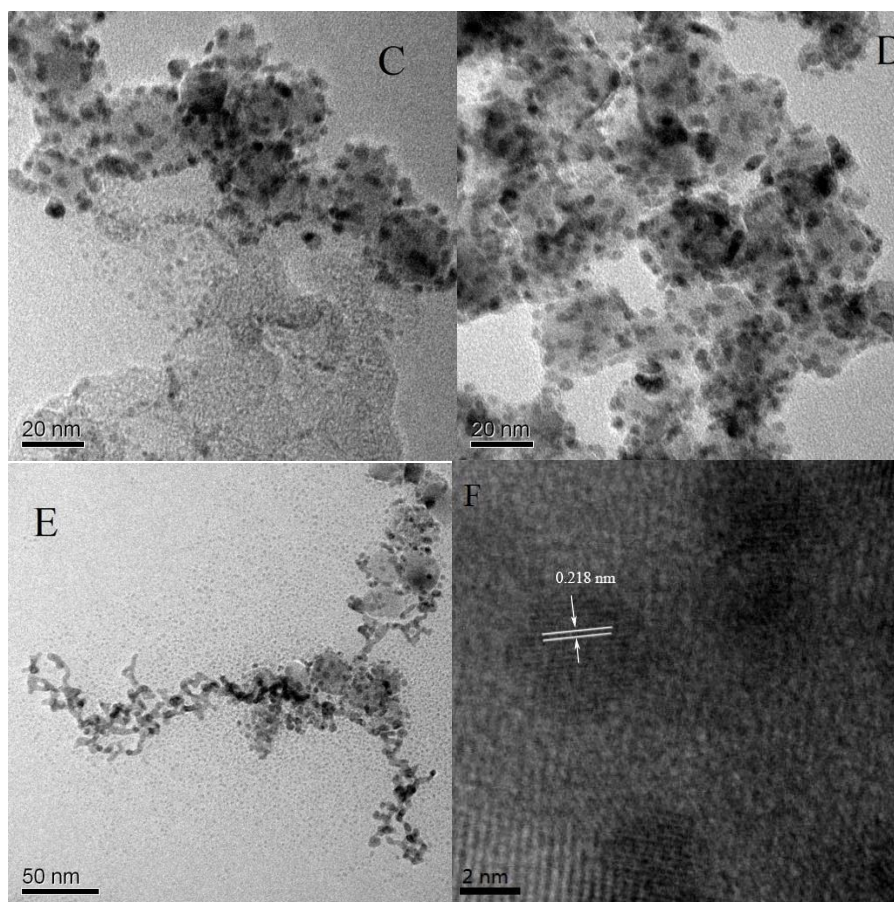
### 3. RESULTS AND DISCUSSION



**Figure 2.** XRD patterns of (a) Pd/TiO<sub>2</sub>(P)-C, (b) PdCu/TiO<sub>2</sub>(P)-C(1:1), (c) PdCu/TiO<sub>2</sub>(P)-C(1:2), (d) PdCu/TiO<sub>2</sub>(P)-C(1:3).

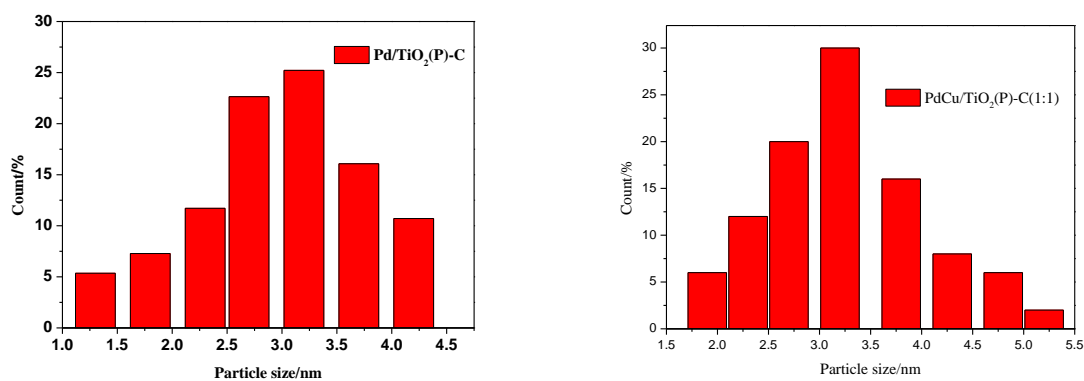
Fig. 2 shows the XRD patterns of the Pd/TiO<sub>2</sub>(P)-C and PdCu/TiO<sub>2</sub>(P)-C catalysts with different mass ratios of Pd and Cu. It was observed from Fig. 2a that the three diffraction peaks at 39.8, 44.9 and 67.9°(2θ) from NP-Pd can be assigned to the (111), (200), and (220) diffractions for a face-centered cubic (fcc) pure Pd respectively (JCPDS standard 05-0681 (Pd))[26]. It should be noticed three kinds of PdCu/TiO<sub>2</sub>(P)-C only show the peak of plane (111) and (200), and the peak of Pd (220) was not observed because the strength is too weak. For each of three PdCu/TiO<sub>2</sub>(P)-C catalysts, (111) and (200) diffraction peaks were located between the values of pure Pd and Cu, which indicated that face-centered cubic PdCu alloy structure has formed[27]. The (111) and (200) diffraction peaks of three PdCu/TiO<sub>2</sub>(P)-C catalysts shift to higher angles with an increase in Cu content compared with the Pd/TiO<sub>2</sub>(P)-C catalyst. This result presents that the lattice parameter of PdCu alloy becomes smaller regularly because smaller Cu atoms have entered into the crystallattice of Pd.

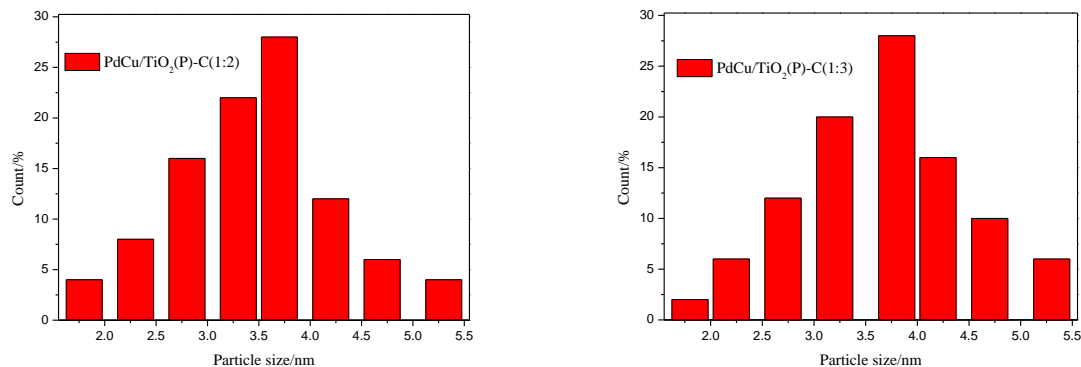




**Figure 3.** TEM images of (A) Pd/TiO<sub>2</sub>(P)-C, (B) PdCu/TiO<sub>2</sub>(P)-C(1:1), (C) PdCu/TiO<sub>2</sub>(P)-C (1:2), (D,E) PdCu/TiO<sub>2</sub>(P)-C(1:3) and HRTEM image of the PdCu/TiO<sub>2</sub>(P)-C(1:1).

Fig. 3 shows TEM images of all four catalysts and HRTEM of PdCu/TiO<sub>2</sub>(P)-C(1:1). It was observed from Fig. 3 that the spherical particles of catalysts possess good dispersion and uniformity. Meanwhile, we also observed a small amount of linear structure in TEM Figure 3(E), which did not appear in other two bimetallic catalysts. Therefore, we hypothesized that using this method of catalyst preparation in the project, the morphology of the catalyst nano-particles will transform into linear structure when the content of Cu rises to a certain extent.

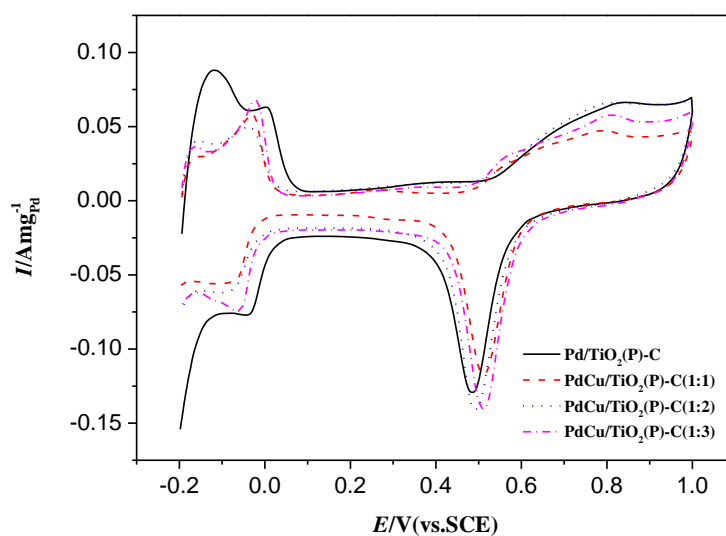




**Figure 4.** Particle size distribution histograms of Pd NPs in Pd/TiO<sub>2</sub>(P)-C, PdCu/TiO<sub>2</sub>(P)-C(1:1), PdCu/TiO<sub>2</sub>(P)-C(1:2), PdCu/TiO<sub>2</sub>(P)-C(1:3).

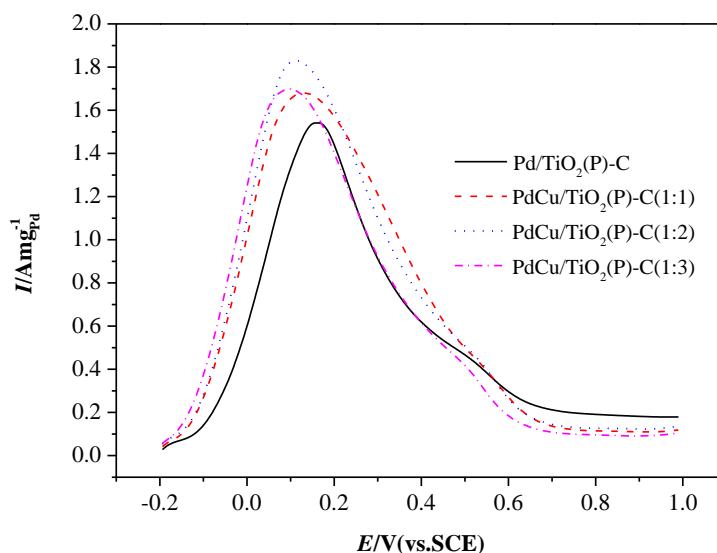
Fig. 3(F) provides a high-resolution TEM (HRTEM) image of PdCu/TiO<sub>2</sub>(P)-C(1:1). The continuous ordered lattice fringes have been seen clearly in Fig. 3(F) and the lattice spacing is calculated to be 0.218 nm, which corresponded to the distance of the (111) crystal planes of fcc Pd<sub>50</sub>Cu<sub>50</sub> alloy [28]. The results of TEM measurement indicated that PdCu alloy structure has formed, which is consistent with the result of XRD patterns.

Fig. 4 provides the corresponding particle size distribution histograms of all four catalysts. According to size distribution histograms, the average sizes of PdCu particles in PdCu/TiO<sub>2</sub>(P)-C(1:1), PdCu/TiO<sub>2</sub>(P)-C(1:2), PdCu/TiO<sub>2</sub>(P)-C(1:3) catalysts are 3.2, 3.5, 3.7 nm respectively. The average size of the Pd particles in the Pd/TiO<sub>2</sub>(P)-C catalyst is 3.0 nm. This result can be explained by that when the content of Cu rises to a certain extent, the morphology of the catalysts will transform into linear structure, thus resulting the increase in the average particle size.



**Figure 5.** CV curves of Pd/TiO<sub>2</sub>(P)-C, PdCu/TiO<sub>2</sub>(P)-C(1:1), PdCu/TiO<sub>2</sub>(P)-C(1:2) and PdCu/TiO<sub>2</sub>(P)-C(1:3) catalysts in a solution of 0.5M H<sub>2</sub>SO<sub>4</sub> at a scan rate of 50 mV·s<sup>-1</sup>.

The cyclic voltammetry (CV) of Pd/TiO<sub>2</sub>(P)-C, PdCu/TiO<sub>2</sub>(P)-C(1:1), PdCu/TiO<sub>2</sub>(P)-C(1:2) and PdCu/TiO<sub>2</sub>(P)-C(1:3) in 0.5 M H<sub>2</sub>SO<sub>4</sub> are shown in Fig.5. It should be noted that all the electrochemical results shown in this article are after 20 cycles in 0.5 M H<sub>2</sub>SO<sub>4</sub> to remove exposed Cu and only leave Pd on the surface. On the one hand, this is done for the purpose of removing impurities on the surface of catalyst and activating the catalyst. On the other hand, it is in order to dissolve Cu on the catalyst surface( known as de-alloy)and form rough surface so that more Pd atoms exposed to the solution, thereby improving the utilization of precious metals[29]. In Fig.5, all catalysts exhibit similar behaviors and we can clearly see the hydrogen adsorption/desorption peaks at -0.20–0V, the PdO<sub>x</sub> reduction peaks at 0.35–0.55V by reverse scan and the peak of PdO<sub>x</sub> formation at higher potentials by forward scan [30]. The absence of Cu oxidation peaks indicates that all the exposed Cu atoms were removed during the CV cycles. In our previous study, the intensity of hydrogen adsorption/desorption peaks in cyclic voltammogram of Pd catalysts in 0.5 M H<sub>2</sub>SO<sub>4</sub> and the strength of PdO<sub>x</sub> reduction peak presented proportional relationship. In other word, greater the intensity of PdO<sub>x</sub> reduction peak show, bigger the intensity of hydrogen adsorption/desorption peaks is[24]. However, in Figure 5, we found three alloy catalysts do not comply with the above rule. The reason may be the different patterns of hydrogen adsorption on the surface of single metal Pd and alloy catalysts. Hydrogen adsorption on Pt metal surface generally is monolayer adsorption, so we can calculate the electrochemical surface area of Pt by hydrogen adsorption/desorption peak areas. The hydrogen adsorption on Pd surface is more complex and not the monolayer adsorption. Therefore, hydrogen adsorption/desorption peak areas could not be used to calculate the electrochemical surface area of Pd. The cyclic voltammetry curves of PdCu alloy catalyst in 0.5 M H<sub>2</sub>SO<sub>4</sub> differ from Pd catalyst can be attributed to the change in the Adsorption pattern of hydrogen due to the interaction between Pd and Cu.



**Figure 6.** CV curves of formic acid electrooxidation on Pd/TiO<sub>2</sub>(P)-C, PdCu/TiO<sub>2</sub>(P)-C(1:1), PdCu/TiO<sub>2</sub>(P)-C(1:2) and PdCu/TiO<sub>2</sub>(P)-C(1:3) catalysts in a solution of 0.5M H<sub>2</sub>SO<sub>4</sub>+0.5M HCOOH at a scan rate of 50 mV·s<sup>-1</sup>.



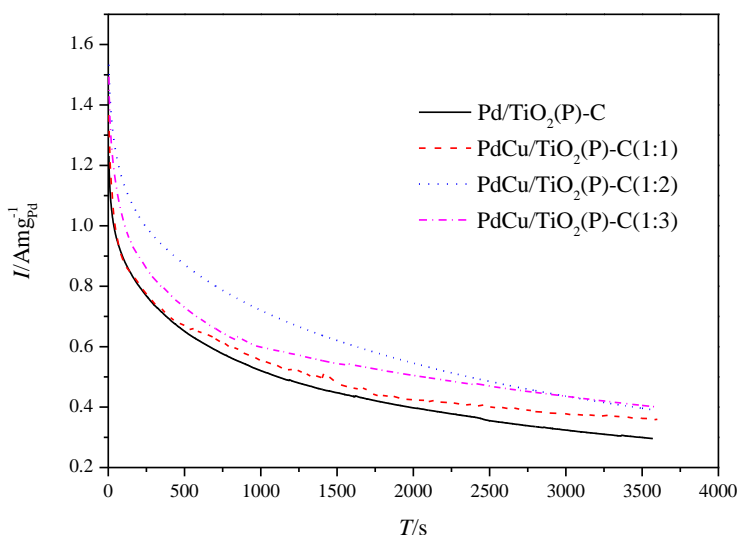
We calculated the electrochemical surface area (ECSA) of catalysts by the charge consumed in PdOx reduction during the cathodic scan. The charge consumed in monolayer oxide reduction was assumed to be  $0.424 \text{ mC}\cdot\text{cm}^{-2}$ . This method is widely accepted in the literature. All these calculated ECSA values are summarized in Table 1. ECSAs of Pd/TiO<sub>2</sub>(P)-C, PdCu/TiO<sub>2</sub>(P)-C(1:1), PdCu/TiO<sub>2</sub>(P)-C(1:2) and PdCu/TiO<sub>2</sub>(P)-C(1:3) are 54.2, 57.5, 59.0, 52.3  $\text{m}^2\cdot\text{g}^{-1}$ . With the content increase of Cu, ECSA first increases, and then decreases. The reason for the increase may be due to that the surface of Pd was more exposed after de-alloying. When the Cu content increases to a certain extent, the morphology of the alloy is changed and the particles begin to gather into linear structure, causing the reduced ECSA.

The activities for the Pd/TiO<sub>2</sub>(P)-C, PdCu/TiO<sub>2</sub>(P)-C(1:1), PdCu/TiO<sub>2</sub>(P)-C(1:2) and PdCu/TiO<sub>2</sub>(P)-C(1:3) toward the formic acid electrochemical oxidation are measured by cyclic voltammetry tests in 0.5 M H<sub>2</sub>SO<sub>4</sub> with 0.5 M formic acid (Fig. 6). The peak current densities in the forward scan for Pd/TiO<sub>2</sub>(P)-C, PdCu/TiO<sub>2</sub>(P)-C(1:1), PdCu/TiO<sub>2</sub>(P)-C(1:2) and PdCu/TiO<sub>2</sub>(P)-C(1:3) are 1.54, 1.68, 1.83 and 1.70  $\text{A}\cdot\text{mg}^{-1}$  respectively. The peak potential of formic acid oxidation on Pd/TiO<sub>2</sub>(P)-C, PdCu/TiO<sub>2</sub>(P)-C(1:1), PdCu/TiO<sub>2</sub>(P)-C(1:2) and PdCu/TiO<sub>2</sub>(P)-C(1:3) are 0.16, 0.13, 0.11, 0.10, respectively. With the content increase of Cu, The peak current densities first increases, and then decreases. This may be mainly due to the decreases of ECSA of PdCu/TiO<sub>2</sub>(P)-C (1:3). The peak potentials of formic acid oxidation on PdCu/TiO<sub>2</sub>(P)-C were shifted negatively compared with that of Pd/TiO<sub>2</sub>(P)-C, which demonstrates that HCOOH is more susceptible to oxidization on the surface of PdCu/TiO<sub>2</sub>(P)-C.

Table 1 also lists the specific activities of all catalysts. Specific activity of catalysts is very important parameter, which can evaluate its catalytic activity. The specific activities of Pd/TiO<sub>2</sub>(P)-C, PdCu/TiO<sub>2</sub>(P)-C(1:1), PdCu/TiO<sub>2</sub>(P)-C(1:2) and PdCu/TiO<sub>2</sub>(P)-C(1:3) are 2.84, 2.92, 3.10, 3.25  $\text{mA}\cdot\text{cm}^{-2}$ , respectively. The specific activities increase with the content increase of Cu. Since the adsorption of CO on Pd in alloy catalysts weakened, more reactive sites release, thereby enhancing the specific activities. When the Cu content is higher, this effect will be greater [31,32].

**Table 1.** Summary of the electrochemical data of Pd/TiO<sub>2</sub>(P)-C, PdCu/TiO<sub>2</sub>(P)-C(1:1), PdCu/TiO<sub>2</sub>(P)-C(1:2), PdCu/TiO<sub>2</sub>(P)-C (1:3) composite catalysts (derived from fig.5 and 6).

Sample	ECSA ( $\text{m}^2\cdot\text{g}^{-1}$ )	Mass activity ( $\text{A}\cdot\text{mg}^{-1}$ )	Specific activity ( $\text{mA}\cdot\text{cm}^{-2}$ )	Peak potential (V)
Pd/TiO <sub>2</sub> (P)-C	54.2	1.54	2.84	0.16
PdCu/TiO <sub>2</sub> (P)-C(1:1)	57.5	1.68	2.92	0.13
PdCu/TiO <sub>2</sub> (P)-C(1:2)	59.0	1.83	3.10	0.11
PdCu/TiO <sub>2</sub> (P)-C (1:3)	52.3	1.70	3.25	0.10



**Figure 7.** The  $i-t$  curves of formic acid electro-oxidation on the Pd/TiO<sub>2</sub>(P)-C, PdCu/TiO<sub>2</sub>(P)-C(1:1), PdCu/TiO<sub>2</sub>(P)-C(1:2) and PdCu/TiO<sub>2</sub>(P)-C(1:3) catalysts at 0.1V in a solution of 0.5 M H<sub>2</sub>SO<sub>4</sub>+0.5 M HCOOH

To further compare the performance and stability of the Pd/TiO<sub>2</sub>(P)-C, PdCu/TiO<sub>2</sub>(P)-C(1:1), PdCu/TiO<sub>2</sub>(P)-C(1:2) and PdCu/TiO<sub>2</sub>(P)-C(1:3), chronoamperometry measurements were carried out in the solution of 0.5 M H<sub>2</sub>SO<sub>4</sub> and 0.5 M HCOOH at 0.1 V for 3600s (see Figure 7). The current densities of formic acid electro-oxidation on the four catalysts change in the similar way, which is declining sharply and then remaining relatively stable. Wherein, the declining tendency reflects catalyst poisoning, which caused by COads adsorbed on the surface of Pd[33]. The current densities of three PdCu/TiO<sub>2</sub>(P)-C catalysts are greater than that of Pd/TiO<sub>2</sub>(P)-C throughout 3600s, which revealed that three PdCu/TiO<sub>2</sub>(P)-C catalysts have superior CO-tolerance ability. After an hour of testing, the current density of Pd/TiO<sub>2</sub>(P)-C, PdCu/TiO<sub>2</sub>(P)-C(1:1), PdCu /TiO<sub>2</sub>(P)-C(1:2) and PdCu/TiO<sub>2</sub>(P)-C(1:3) remain 22.06, 22.78, 23.53, 24.22 % of the initial. This result suggests that stability of three PdCu alloy catalysts is higher than a single metal Pd, the reason may be that the adsorption of CO on Pd in alloy catalyats weakened.

#### 4. CONCLUSION

Pd/TiO<sub>2</sub>(P)-C, PdCu/TiO<sub>2</sub>(P)-C with different mass ratio of Pd and Cu are successfully synthesized by the self-assembly and then in situ deposition on the surface of TiO<sub>2</sub> modified by PDDA. TEM micrographs showed that Pd and PdCu nanoparticles were uniformly dispersed on the surface of TiO<sub>2</sub>. when the content of Cu rises to a certain extent, the morphology of the catalyst nanoparticles will transform into linear structure. By XRD, HRTEM pattern, alloy structure of PdCu was confirmed. Electrochemical measurements indicated that CuPd alloy catalysts have higher and more stable activities of formic acid oxidation compared with the Pd/TiO<sub>2</sub>(P)-C catalyst. The effect of

different ratios of PdCu on catalyst activity was also discussed in this research. Taken all together, PdCu/TiO<sub>2</sub>(P)-C(1:2) catalyst presents the best catalytic activity and stability for the formic acid electro-oxidation.

#### ACKNOWLEDGEMENTS

This research was supported by the National undergraduate training programs for innovation (201510532035) and the Hunan Provincial Natural Science Foundation of China (13JJ5018)

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